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UC-2993

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METALS DIVISION

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To (Name) Mr. R. G. Woolery
Division
Location Building 94 - Niagara

Date July 2, 1976
Originating Dept. Technology
Answering letter date

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Subject Supervisbestos, Wetted Product, Improved Quality

With reference to Bill Thurber's letters of June 1 and June 8 on improving the Supervisbestos, there are two suggestions which may be worth considering for producing a wetted product and for improving product quality.

1. Wetted product

The possibility exists for making a dust-free product with equipment already available at the plant. The procedure suggested is to blend S V filter cake with dry pellets using the Lancaster mixer from the RG-400 process. By this technique, the Lancaster mixer would be used to crush the dry pellets to a small size (for low settling velocity in the user's mud tank) and the generated fines are simultaneously blended and agglomerated with the wet filter cake to eliminate the dust. A secondary benefit of the system is that the filter cake drying load is reduced in proportion to the amount of water left in the final product.

Tests at Niagara Falls with High Purity in a Mix-Muller show that 4 parts by weight filter cake with 6 parts pellets (20% final moisture) yields a product that is dust-free. The mixture is also free-flowing and it should be amenable to bagging with the Force-Flow machines.

The tests also indicated that the moisture requirement increases with the degree of pellet attritioning since the filter cake selectively agglomerates only with the fines and the larger particles of asbestos remain dry. For this reason, it would be necessary to control the degree of pellet crushing in the Lancaster after the initial cake blending period of the batch operation.

The wetted product could be packaged in plastic-lined bags with the auger packer or in paper bags by the Force Flow units and overwrapped using the RG-244 packages.

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2. Improved Supervisbestos Quality

The viscosity promotion of Supervisbestos is directly related to the quantity of liberated fiber contained in the pellets (Packaged Available Fiber quality control test). The P.A.F. ranges at 55 to 60% for S V. For HPP, the P.A.F. is 75 to 80%.

The Supervisbestos fiber is liberated by open circuit grinding and 55 to 60% yield is a reasonable maximum. The liberated fiber yield may be increased, however, by closing the grinding circuit. This could be done by means of the primary refining cyclones and recycling the cyclone underflow to the Fitz fiber mills for regrinding.

Closing the grinding circuit will increase filtration time due to lower feed solids and higher fiber content. It should, however, allow the S V to approach HPP in P.A.F. content and provide a 30 to 40% increase in viscosity performance index.

J. E. Skvarla

JES:sjc

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